

Amendments to the Specification

Please replace the paragraph appearing on page 16, lines 6-7, with the following amended text:

in which R₂ is a moiety having a composition selected from the group of consisting of formula (A), formula (B), formula (C), and mixtures thereof,

Please replace the paragraph appearing on page 24, lines 7-8, with the following amended text:

in which R₂ is a moiety having a composition selected from the group of consisting of formula (A), formula (B), formula (C) and mixtures thereof,

Please replace the paragraph appearing on page 27, line 32, to page 28, line 9, with the following amended paragraph:

An asymmetric hollow-fiber membrane of P84 was spun from a solution of 30 % P84, 9.0 %. Tetramethylene sulfone and 1.5 % acetic anhydride in N-methylpyrrolidinone (NMP) with methods and equipment as described in U.S. Patent Nos. 5,034,024 and 5,015,270. The nascent filament was extruded at a rate of 180 cm³/hr through a spinneret with fiber channel dimensions of outer diameter 559 µm, and inner diameter equal to 254 µm at 75°C. A fluid containing 85% NMP in water was injected in-to into the bore of the fiber at a rate of 33 cm³/hr. The nascent fiber traveled through an air gap of 5 cm at room temperature into a water coagulant bath at 24°C and the fiber was wound up at a rate of 52 m/min.

Please replace the paragraph appearing on page 30, line 13, with the following amended paragraph:

The membrane performance was tested in the same manner as described for Example 1a. The average performance of a P84 based Example 1e permeators permeator was 27.7 GPU carbon dioxide permeance, and carbon dioxide/nitrogen selectivity 19.5.

Please replace the paragraph appearing on page 30, line 19, with the following amended paragraph:

The membrane performance was tested in the same manner as described for Example 1a except that the feed pressure was 8.4 MPa (1200 psig). The average performance of a P84 based Example 1f ~~permeators~~ permeator was 10.6 GPU carbon dioxide permeance, and carbon dioxide/nitrogen selectivity 18.0.

Please replace the paragraph appearing on page 31, line 10, with the following amended paragraph:

The water-wet fibers were dehydrated and dried as described in Example 1a, and fabricated into permeator modules. The modules were further post-treated and dried in a vacuum oven at 100°C for 16 hours and then tested as in Example 1f. The average performance of two permeators was 3.6 GPU for carbon dioxide permeance, and a carbon dioxide/nitrogen selectivity 13.0. This initial permeance is approximately ~~about~~33% ~~about~~33% of that of Example 1f.

Please replace the paragraph appearing on page 34, line 20, with the following amended paragraph:

Permeator modules from Example ~~Examples~~ 1d, and 1e were tested under the conditions of Example 1a and Comparative Example 1 with the exception that toluene at a concentration of 150 ppm for duration of 19 days and then toluene at a concentration of 450 ppm for duration of 24 days was injected in the feed. The toluene injection was then stopped and the permeator performance was finally measured again at the initial hydrocarbon-free conditions for a further 12 days. The change in CO₂ permeance over the duration of the test is shown in Table 5.